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On Novel Marangoni Flows

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Interfacial Fluid Dynamics

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Interfacial Energy \sim Bulk Energy \Rightarrow Something interesting

Interfacial Fluid Dynamics

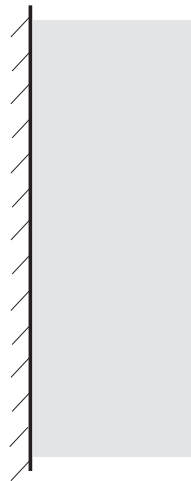
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Simplest Geometries

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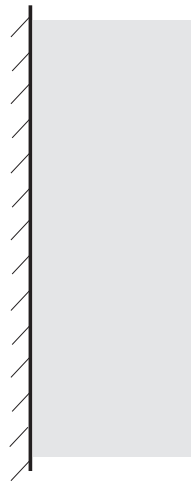


Thin films

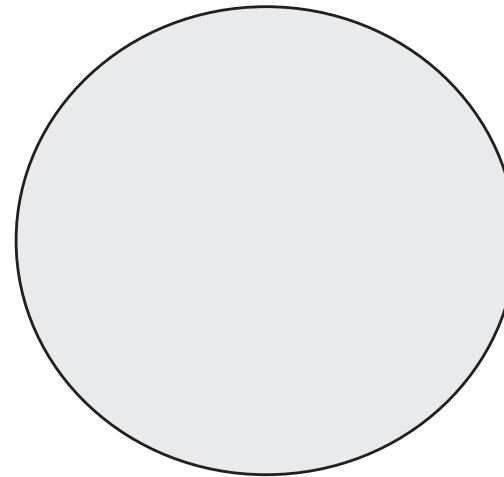
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Drops/Bubbles

Outline

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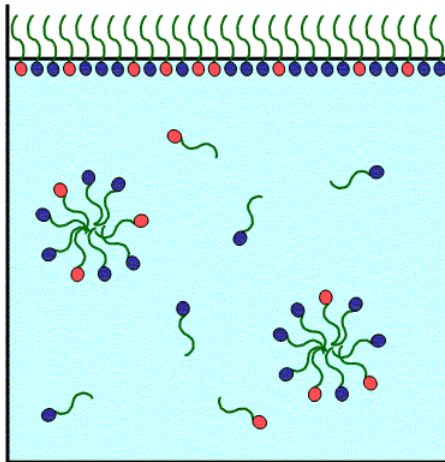
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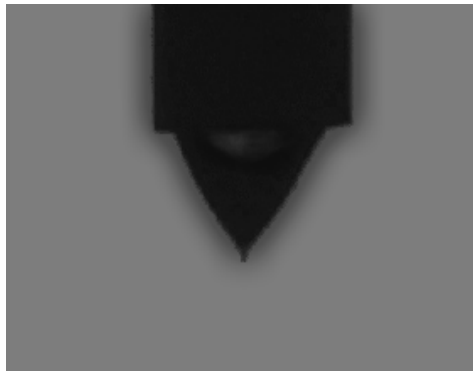


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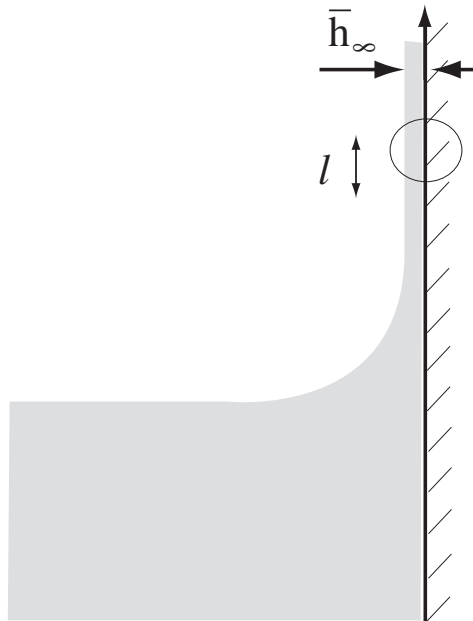


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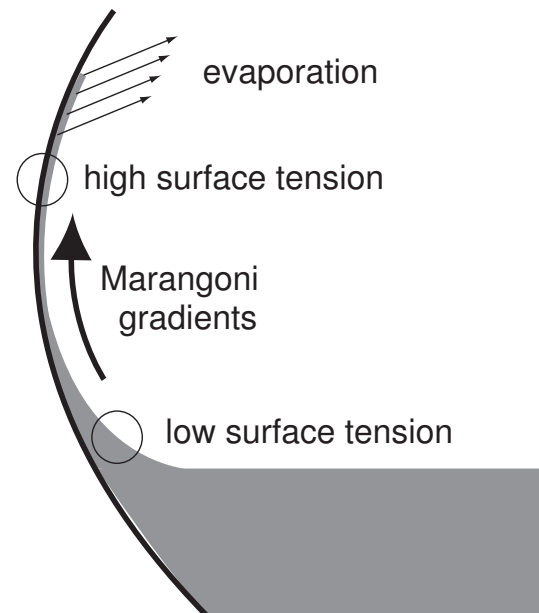
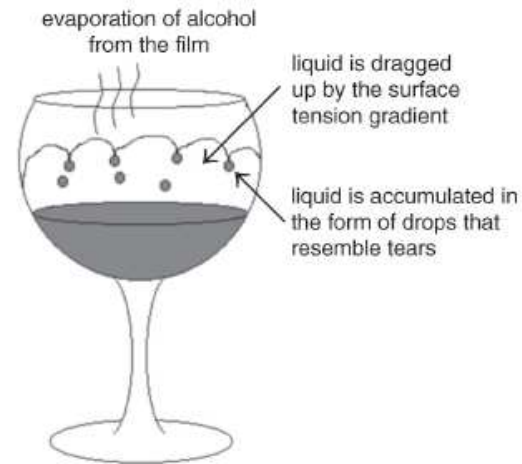
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- Conclusions

What are the Marangoni effects^a?



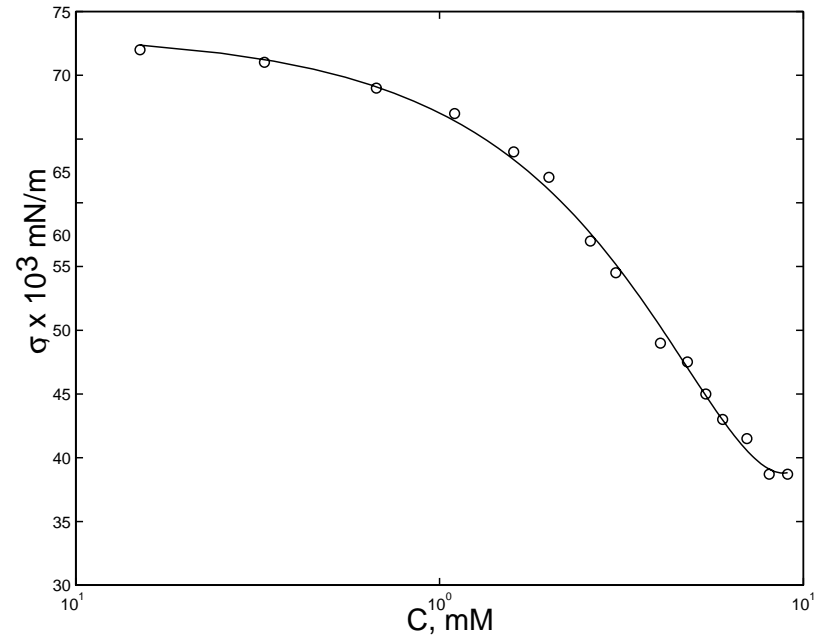
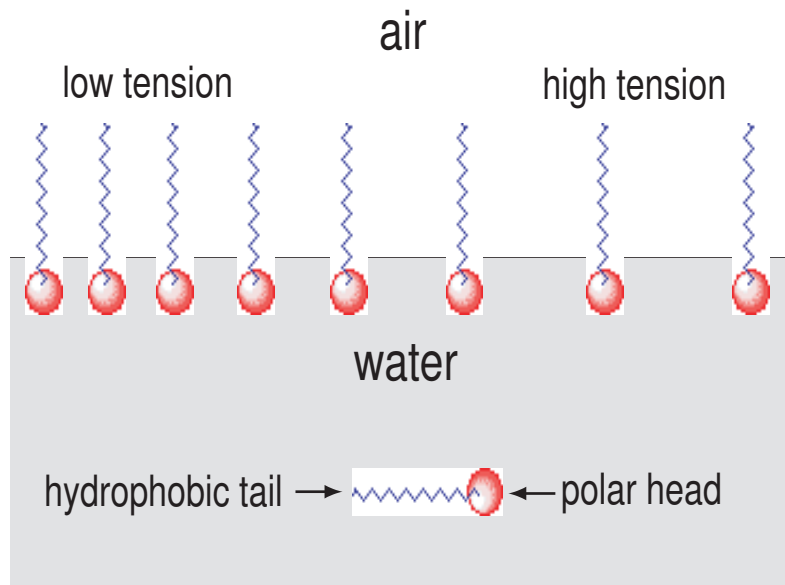
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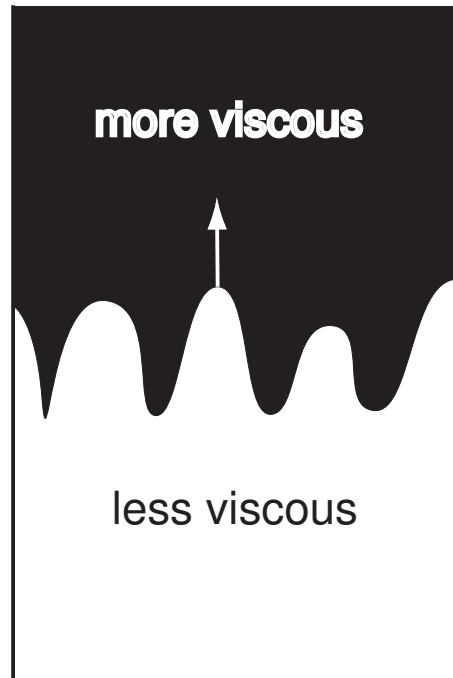
Basic physics of surfactants



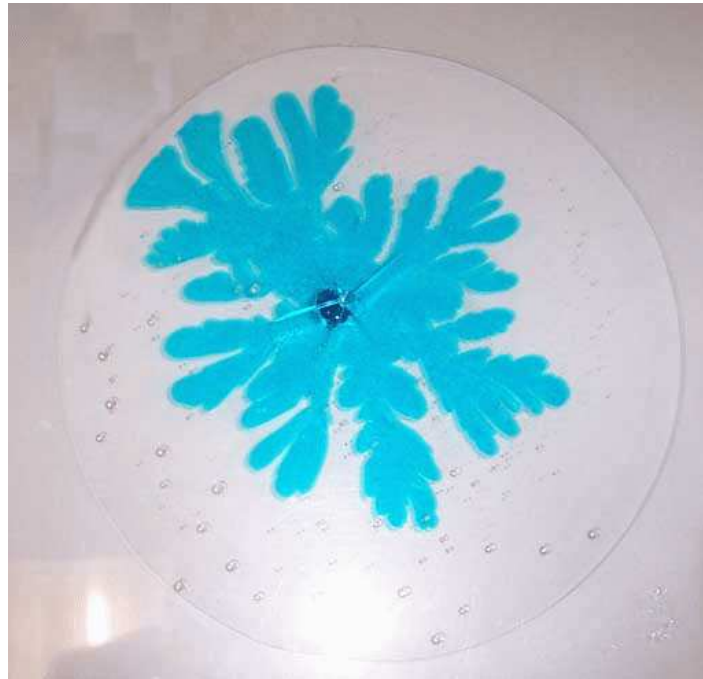
North American surfactant consumption in consumer products was 4.375 billion lbs last year, valued at \$3.6 billion.

Part I. Fingering in a Hele-Shaw cell

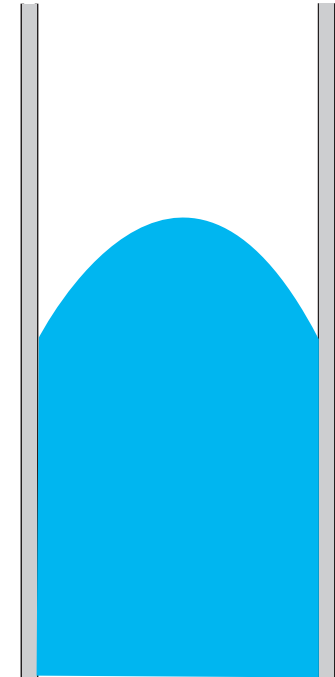
Saffman-Taylor instability^a



Planar cell.



Circular cell.



Thin dimension.

Darcy's law: $\mathbf{u} = -\frac{b^2}{12\mu} \text{grad } p$, $\text{div } \mathbf{u} = 0 \implies$ 2D effect

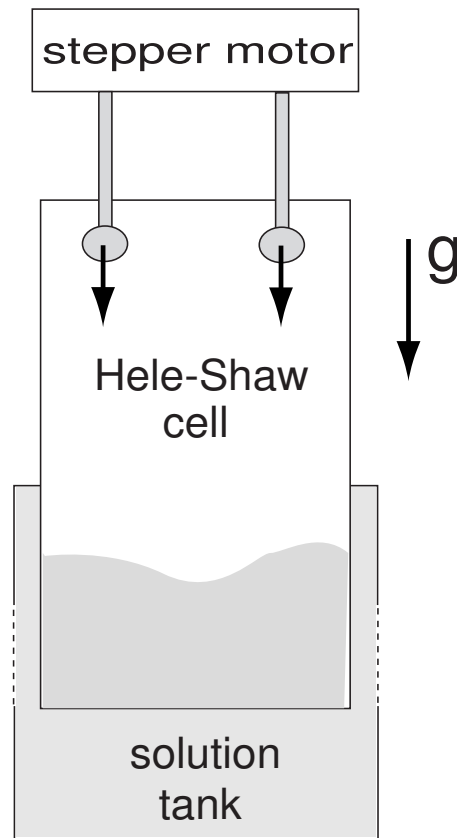
^aHill (1952), Saffman & Taylor (1958), Chuoke *et al.* (1959)

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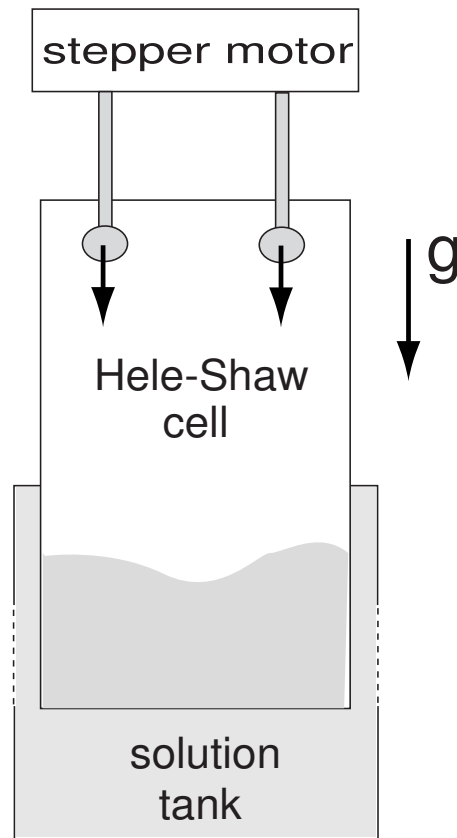
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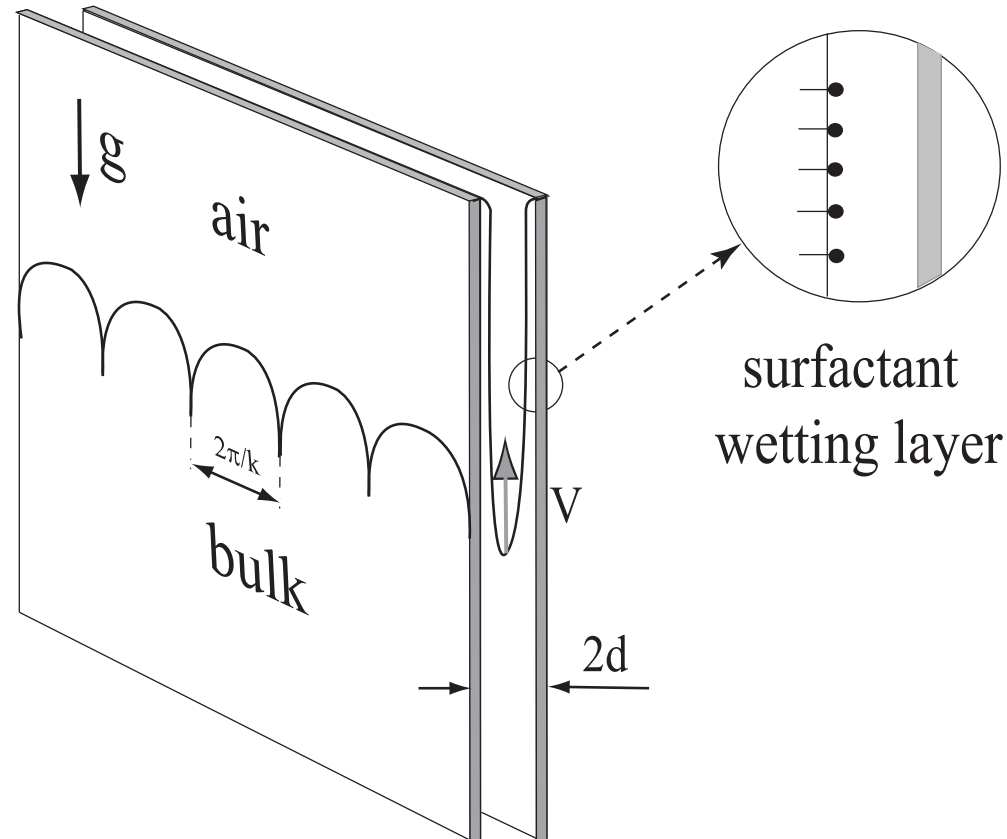
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- Chan (2000) has proposed a **linear stability analysis** by considering another non-physical state equation for the surface tension – a linear dependence on the deformation of the interface.

Surfactant-driven fingering^a

Hele-Shaw cell



^aKrechetnikov & Homsy, JFM (2004); Fernandez, Krechetnikov & Homsy, JFM (2005)

Fingering pattern of RST instability



A Hele-Shaw cell with gap of width $300 \mu m$ is driven at a speed of 3.8 cm/s into a 4.0 mM solution of SDS^a.

^aSodium Dodecyl Sulphate, which is widely used in soaps, detergents, *etc.*

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 - the surfactant concentration and properties (material and kinetics)
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 - the substrate properties (wettability, smoothness)

The core of the problem

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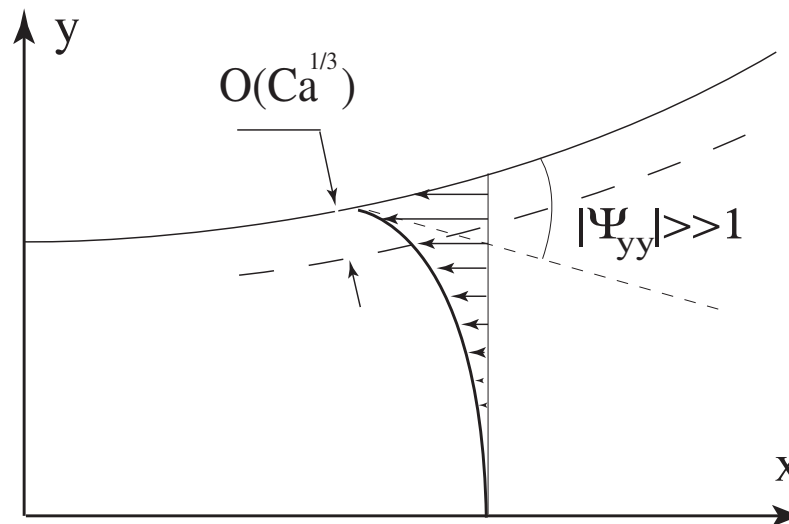
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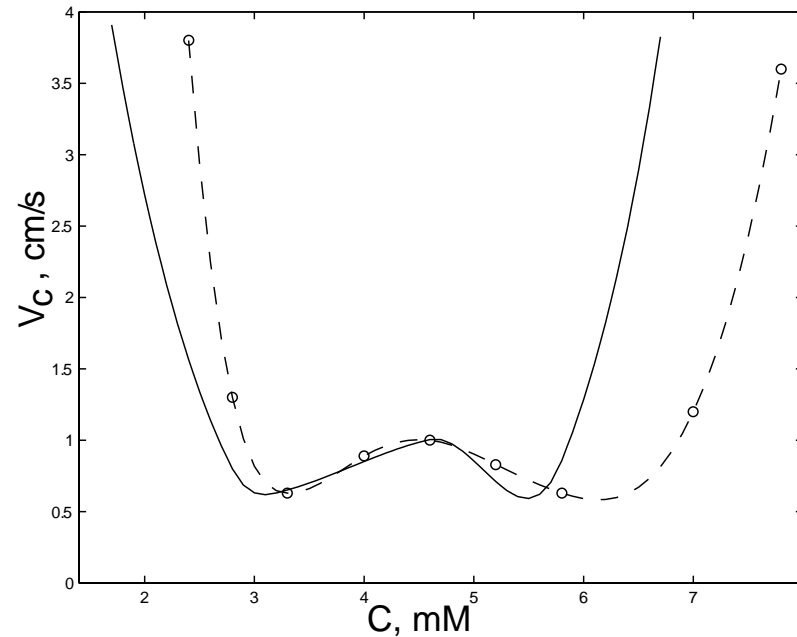
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- Commonly used conjecture: $\gamma = Ca^{2/3} \tilde{\gamma}$ (trace amounts);
- Our conjecture: singular perturbation case with an inner scale $y = Ca^{1/3} \tilde{y}$ (order one surfactant effect)



Conclusions on Part I

Marginal stability & comparison with experiment



(solid line – theory; dashed line – experiment)

The elementary interpretation: *the instability is due to thickening of the wetting layer caused by significant Marangoni stresses, which originate in the accumulation of surfactants in the cap region.*

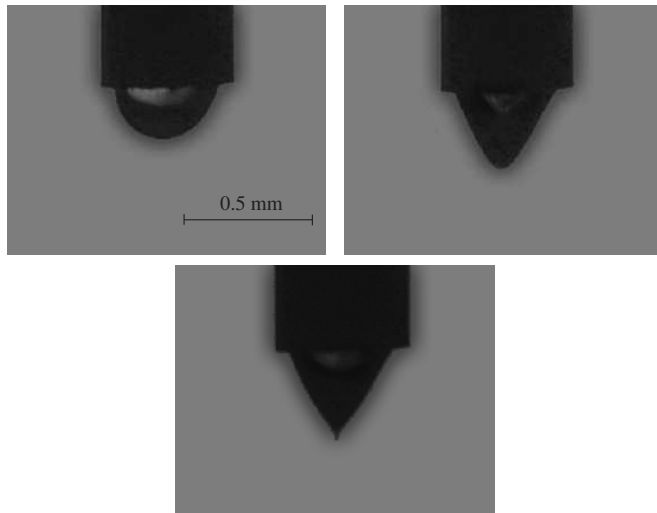
Part II. Amazing drop

Discovered^a in the course of pendant drop measurements with acid/alkaline reaction at the oil/water interface.

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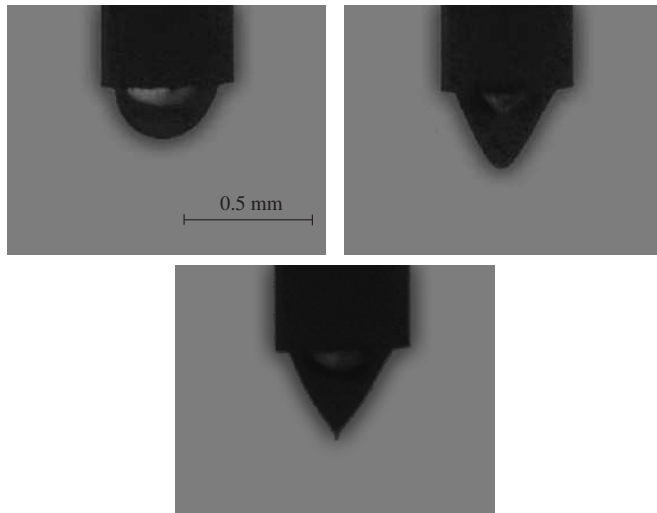


Nonlinear oscillations of a
pendant drop shape

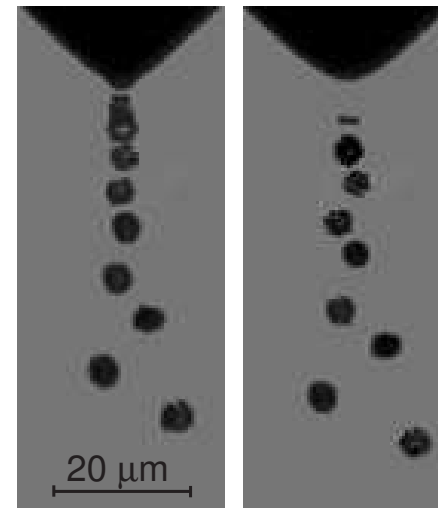
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Nonlinear oscillations of a pendant drop shape



Tip-streaming and droplets splitting

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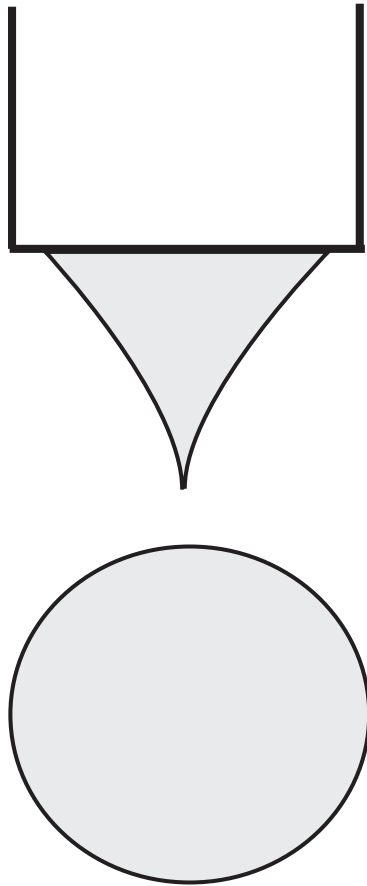
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- **tip-streaming** – formation of the conical drop shape with pointed ends and ejection of very small, $4 \mu m$, droplets from the pointed ends;
- **droplet separation** – organized motion, when one ejected droplet moves to the right, while the subsequent one moves to the left.

Driving mechanism

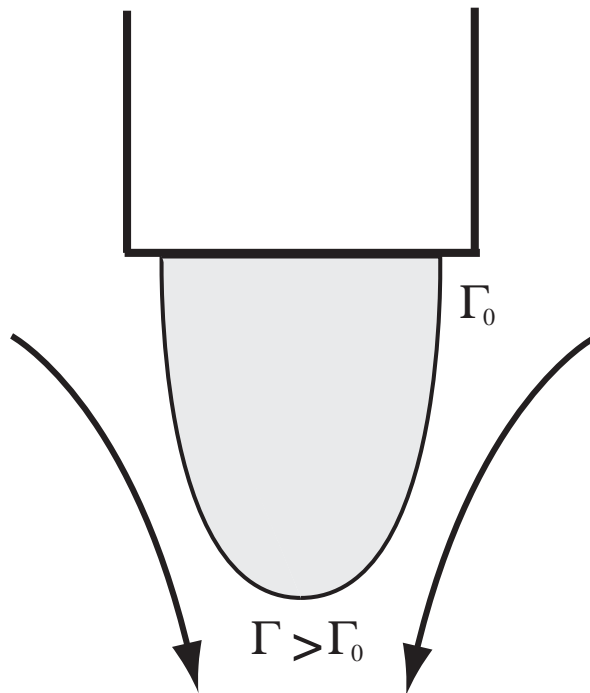
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(t) the *first drop effect* – detachment of a big drop under gravity leading to extensional flow;

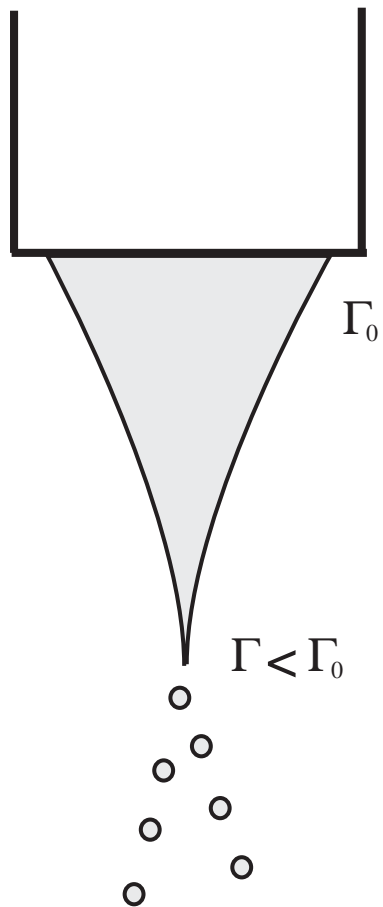


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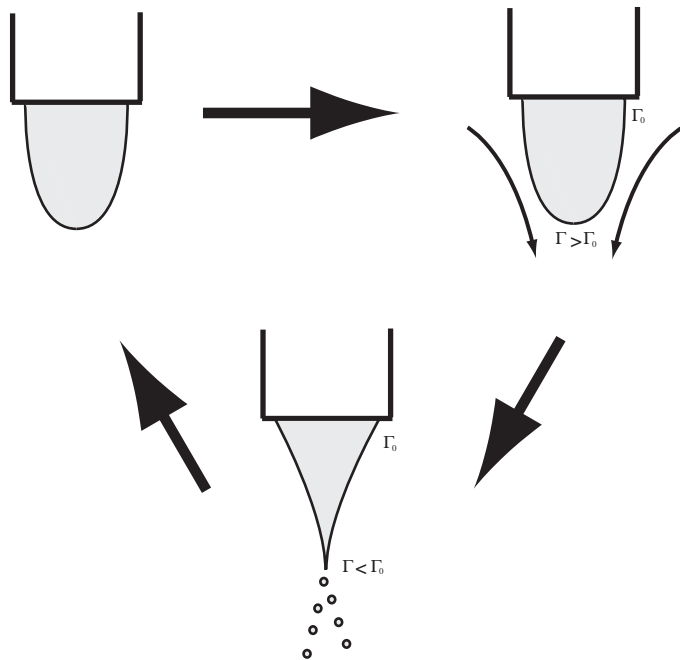


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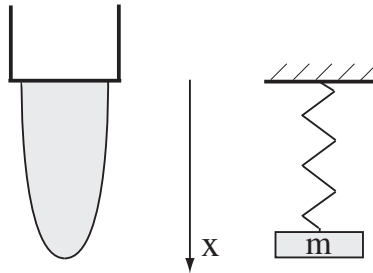
(i) sweeping surfactant towards the tip of a new pendant drop;

(ii) bursting, which removes surfactant from the drop;

(iii) the surfactant concentration gradient between the top and the tip of the drop so created drives Marangoni flow.

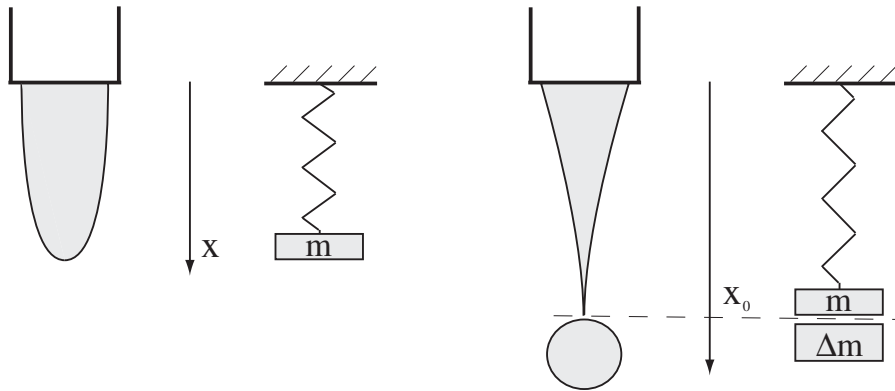
Predecessor: leaky faucet model

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Before detachment

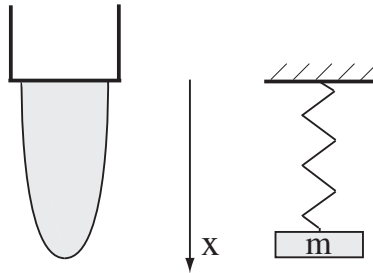
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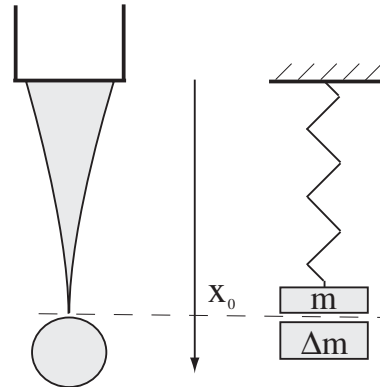
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After detachment

Mass-Spring model

$$\frac{dx}{dt} = v,$$

$$\frac{d(mv)}{dt} = m - (x + bv),$$

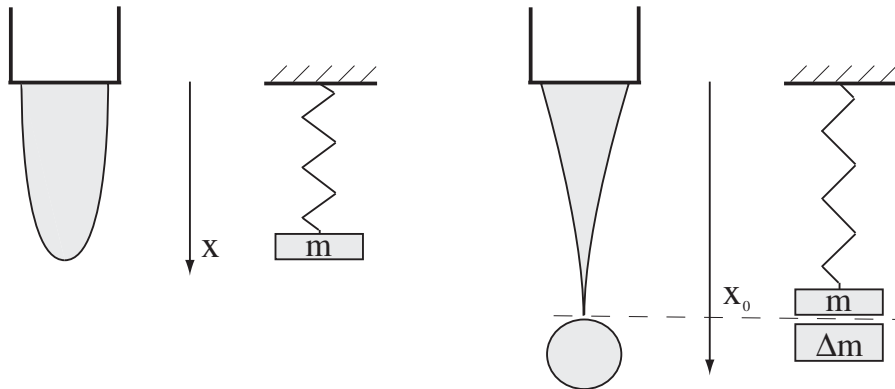
$$\frac{dm}{dt} = r,$$

$$x = x_c : \Delta m = \alpha m_c v_c,$$

$$\Delta x = \beta \frac{\Delta m^{4/3}}{m_c}.$$

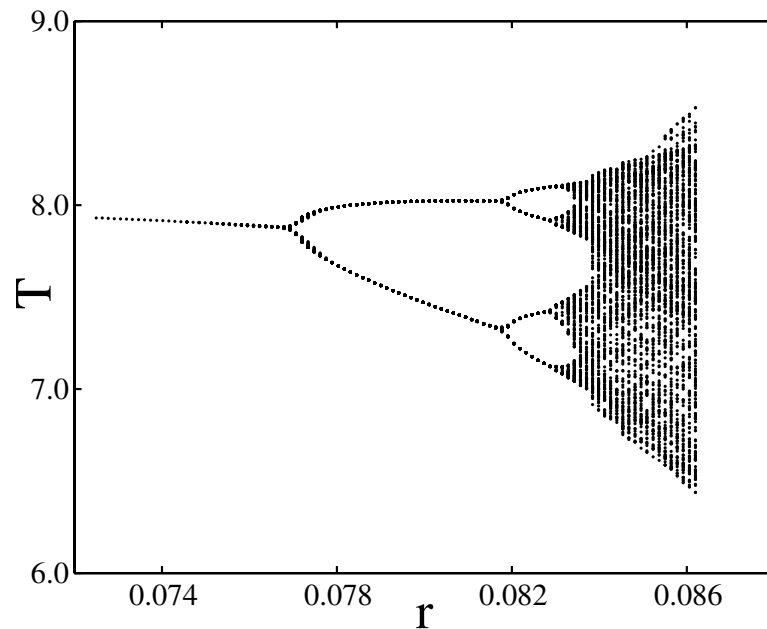
Shaw *et al.* (1984,1985).

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Relaxation oscillator model

The mathematical model:

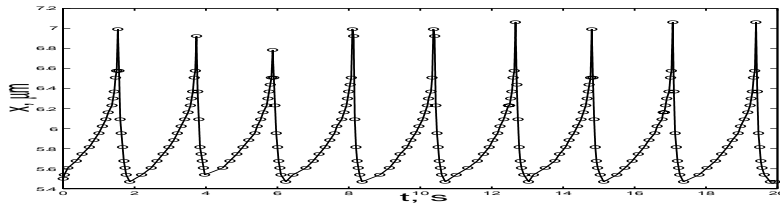
$$M \frac{d^2 x}{dt^2} = \underbrace{Mg}_{\text{gravity}} - \underbrace{b \frac{dx}{dt}}_{\text{friction}} - \underbrace{k(\Gamma) x}_{\text{surface tension}},$$

$$\frac{d\Gamma}{dt} = R, \quad \& \quad \Gamma = \Gamma_c : \quad \Gamma = \Gamma_c - \Delta\Gamma.$$

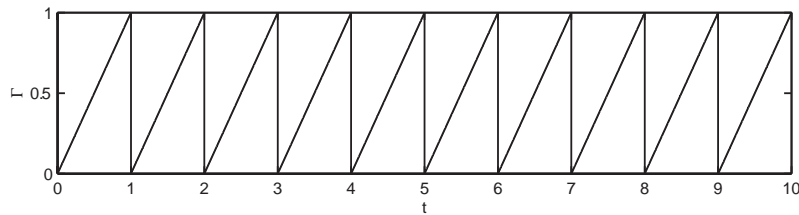
Control parameter: chemical reaction rate R/R_0 with

$$R_0 = 0.29 \cdot 10^{-5} \text{ mol m}^{-2} \text{ s}^{-1}.$$

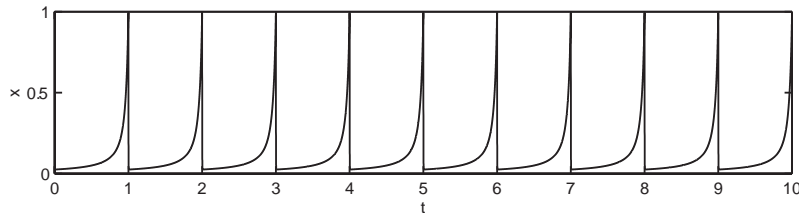
Dynamics of the pendant drop



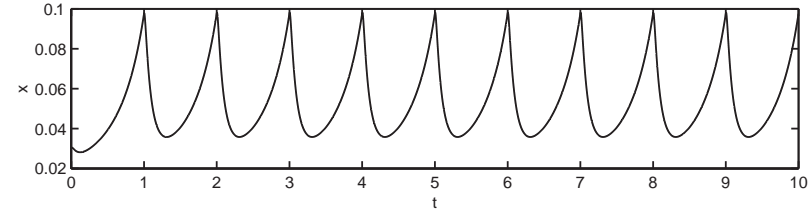
Experiments: tip dynamics.



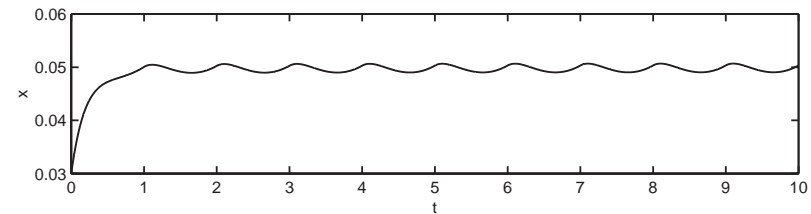
Dynamics of surfactant surface concentration.



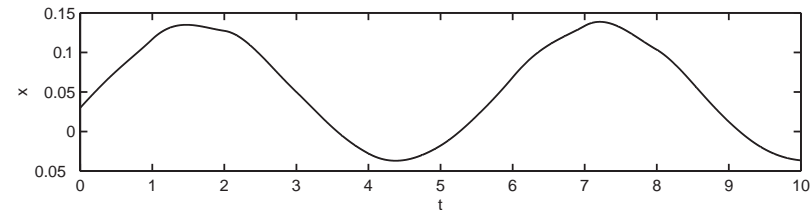
Slow reaction, $R_0/R = 1$: negligible dissipation.



Fast reaction, $R_0/R = 0.01$.

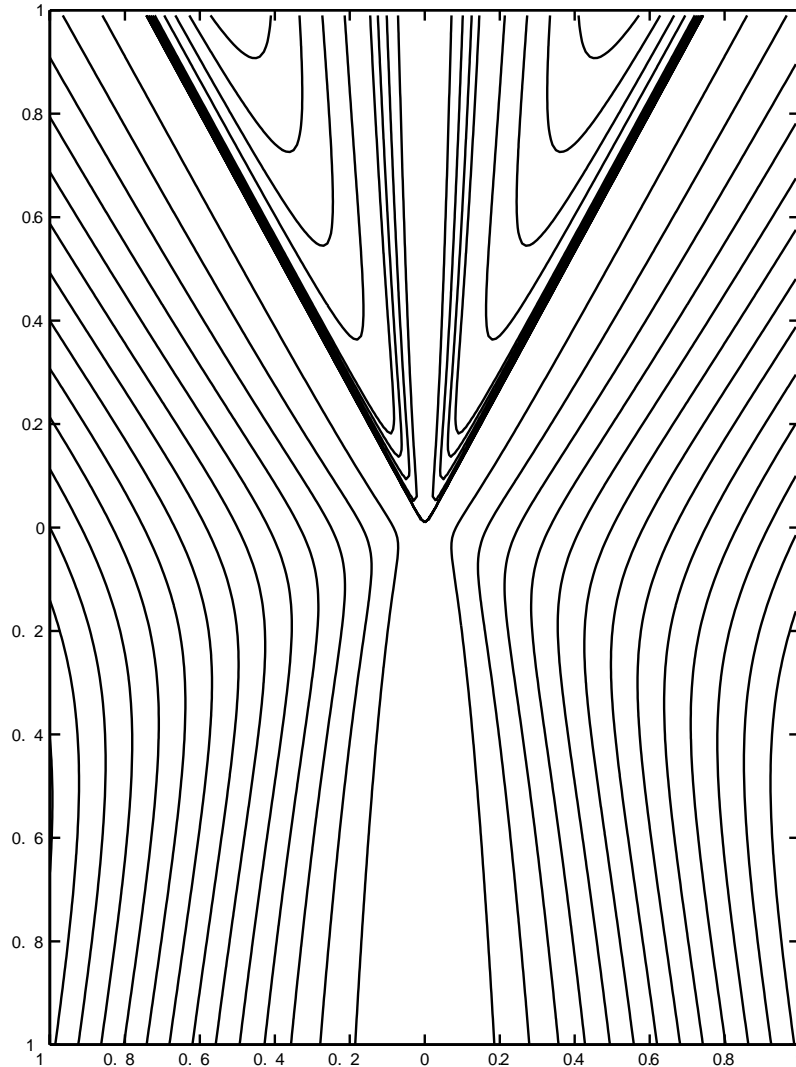


Fast reaction, $R_0/R = 0.0005$: steady tip-streaming.



Fast reaction, $R_0/R = 0.0005$: negligible dissipation.

Steady tip streaming self-similarity



For simplicity, we consider

$$We_1 \ll We_2 \ll 1, We = \rho\sigma_0 d / \mu^2,$$

self-similar solution is defined by

$$\Psi = r\varphi(x), \quad \sigma = \frac{\epsilon}{r}; \quad p = \frac{\pi(x)}{r^2},$$

where $\epsilon = \sigma_{min}$, $x = \cos \theta$, and Ψ is a Stokes stream function in

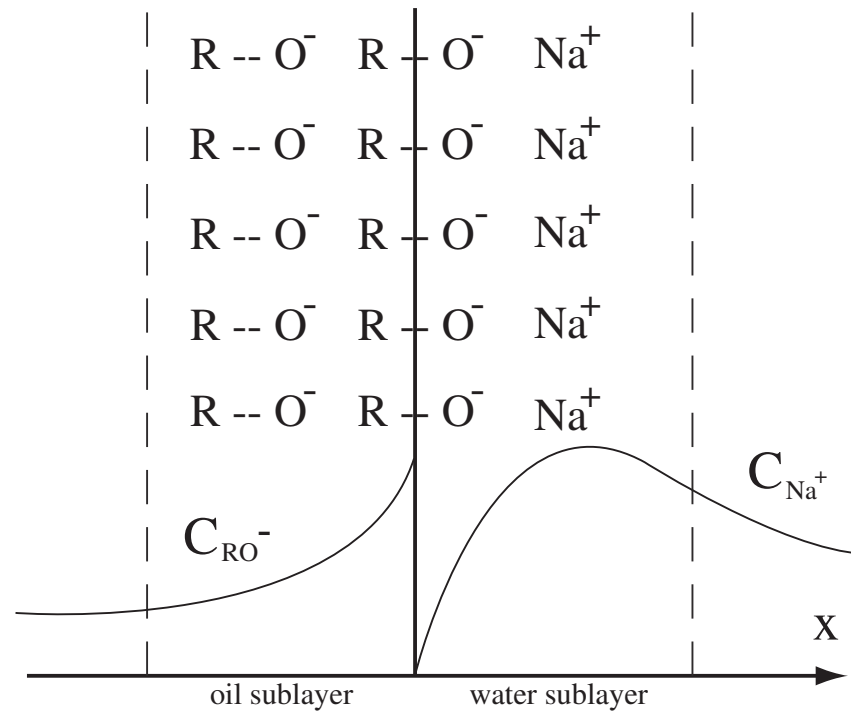
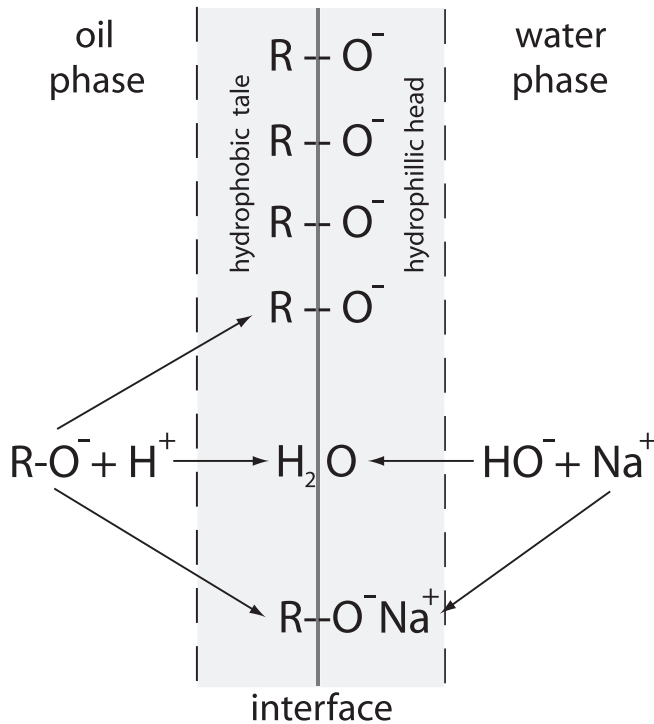
$$x' = r \sin \theta \cos \varphi, \quad y' = r \sin \theta \sin \varphi,$$

$$z' = r \cos \theta,$$

with $\theta \in [0, \pi]$, $\varphi \in [0, 2\pi]$.

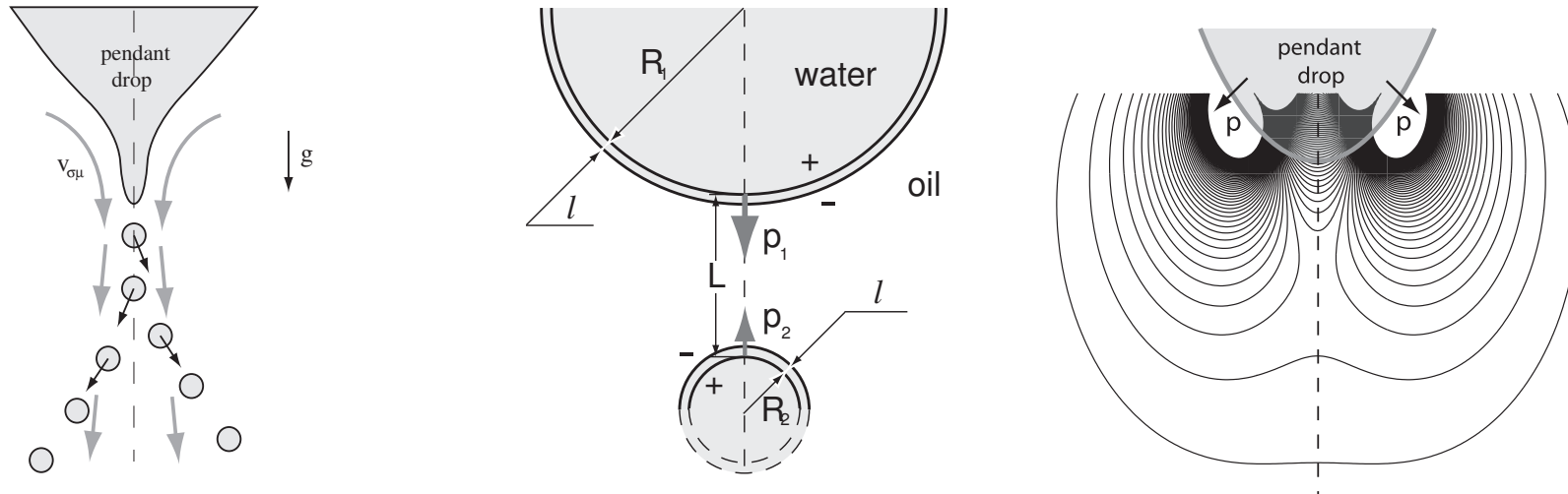
Electrostatic interaction

The interfacial reaction is:



Double layer thickness: $\delta x \sim h^w \sim \left[\frac{\epsilon_0 \epsilon^w}{e^2} \frac{k_B T}{C_{Na^+}^\infty} \right]^{1/2} \sim 10^{-8} m.$

Mechanism of droplets splitting



Schematics of the droplets splitting.

Dipole-dipole interaction of the drops.

Equipotentials of the electric field.

$$F_{p_1-p_2} = \frac{6}{4\pi\epsilon_0\epsilon^o} \frac{p_1 p_2}{L^4}, \text{ where } p_i = 2\pi e R_i^2 \Gamma^{max} N_A h^w.$$

$$F_{p_1-p_2} \sim 0.5 \cdot 10^{-7} \text{ N}, \quad F_{p_2-p_2} \sim 1.0 \cdot 10^{-6} \text{ N};$$

$$F_{st} \sim 6\pi\mu^o R_2 v_{\sigma\mu} \sim 0.5 \cdot 10^{-6} \text{ N}.$$

Conclusions on Part II

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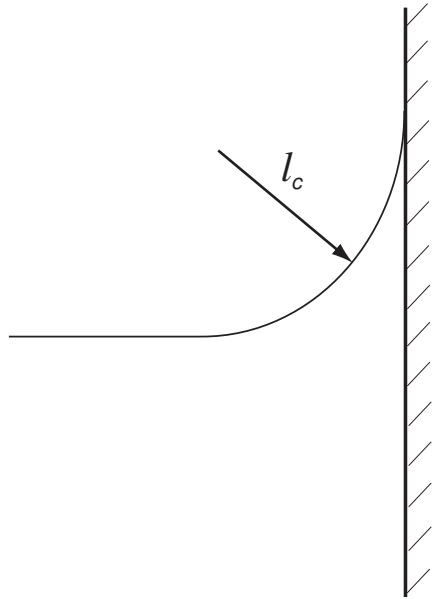
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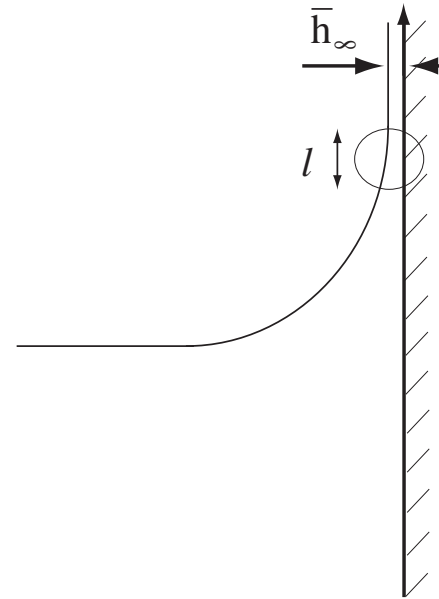
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- The phenomenon of a tip-streaming – a **singularity** responsible for **periodicity** of the phenomenon.
- Electrostatic interactions creates a specific **flow pattern** in which dipole-dipole interactions equilibrate with Stokes drag.

Part III: Landau-Levich problem^a



Static wetting



Dynamic wetting

$$\mu \frac{U}{\bar{h}_\infty^2} \sim \frac{\sigma/l_c}{l}, \quad \frac{\bar{h}_\infty}{l^2} \sim l_c^{-1} \implies \bar{h}_\infty \sim l_c Ca^{2/3} \text{ and } l \sim l_c Ca^{1/3}$$

^aKrechetnikov & Homsy, Phys. Fluids (2005) and JFM (2005).

Landau-Levich problem: milestones

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Clean interface case:

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Landau-Levich problem: milestones

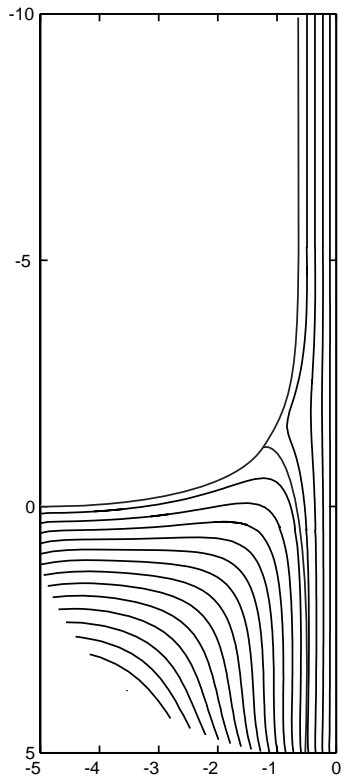
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- Experimental prediction of $2/3$ law by Morey (1940)
- Theoretical derivation of $2/3$ law by Landau & Levich (1942)

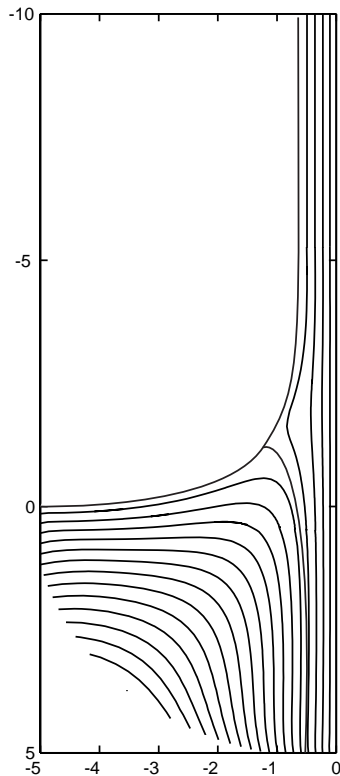
Surfactant interface case:

- Coating in circular tubes by Bretherton (1961)
- Coating flat substrates by Groenveld (1970)
- Fiber coating by Ramdane & Quéré (1997), Shen *et al.* (2002)
- **deviations:** film thickening

Film thickening due to surfactants

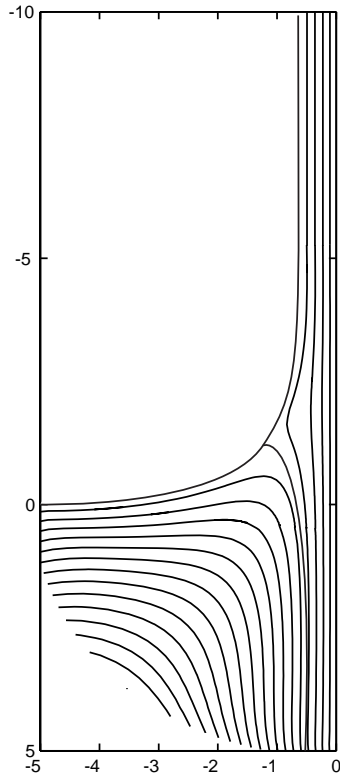


Film thickening due to surfactants



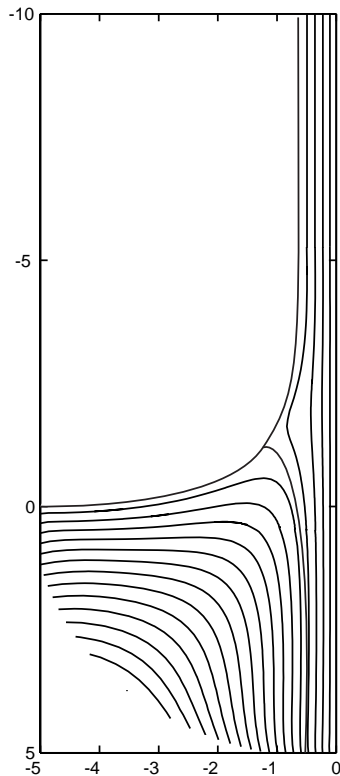
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Film thickening due to surfactants



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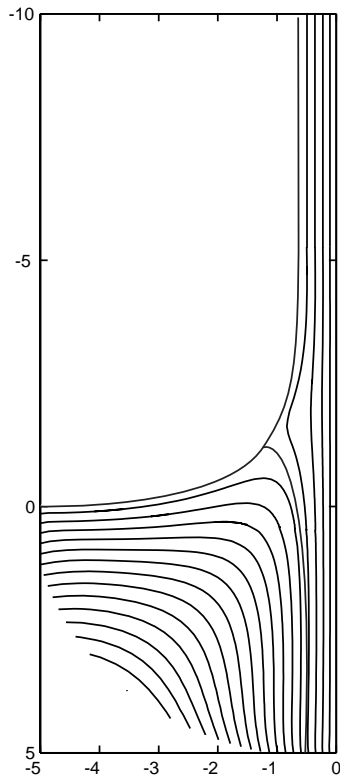
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Film thickening due to surfactants



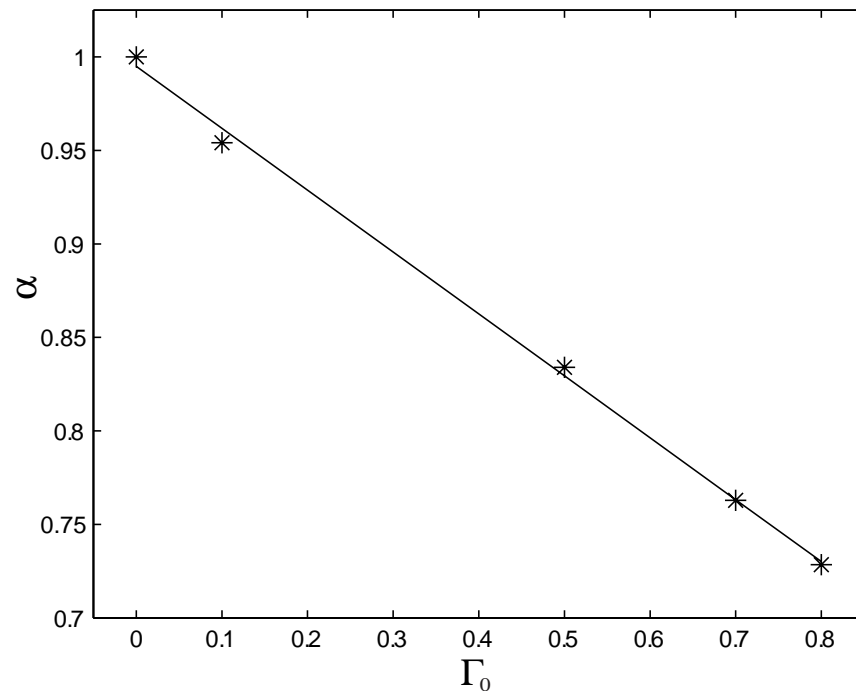
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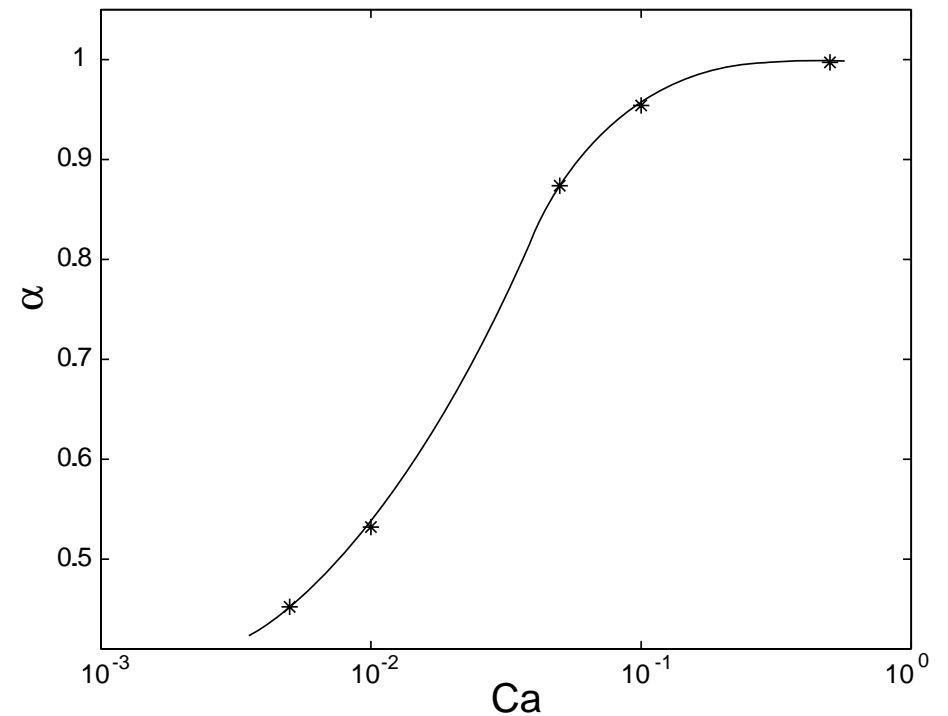
Our goal: to challenge the general belief and asymptotic theories.

Theory: surfactant interface case

Thinning factor $\alpha = \bar{h}_\infty / \bar{h}_\infty^{\text{theory}}$

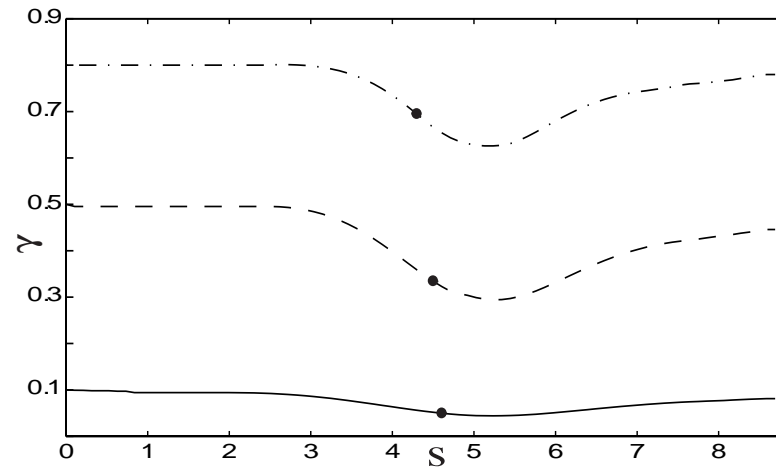
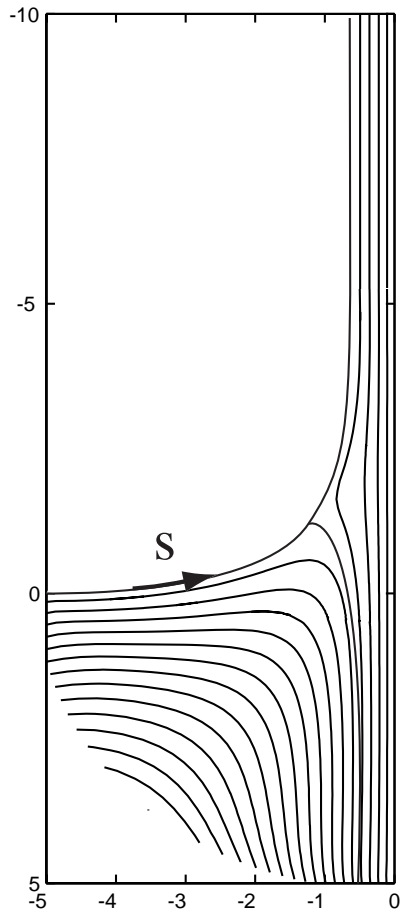


Dependence on Γ_0 for $Ca = 10^{-1}$.



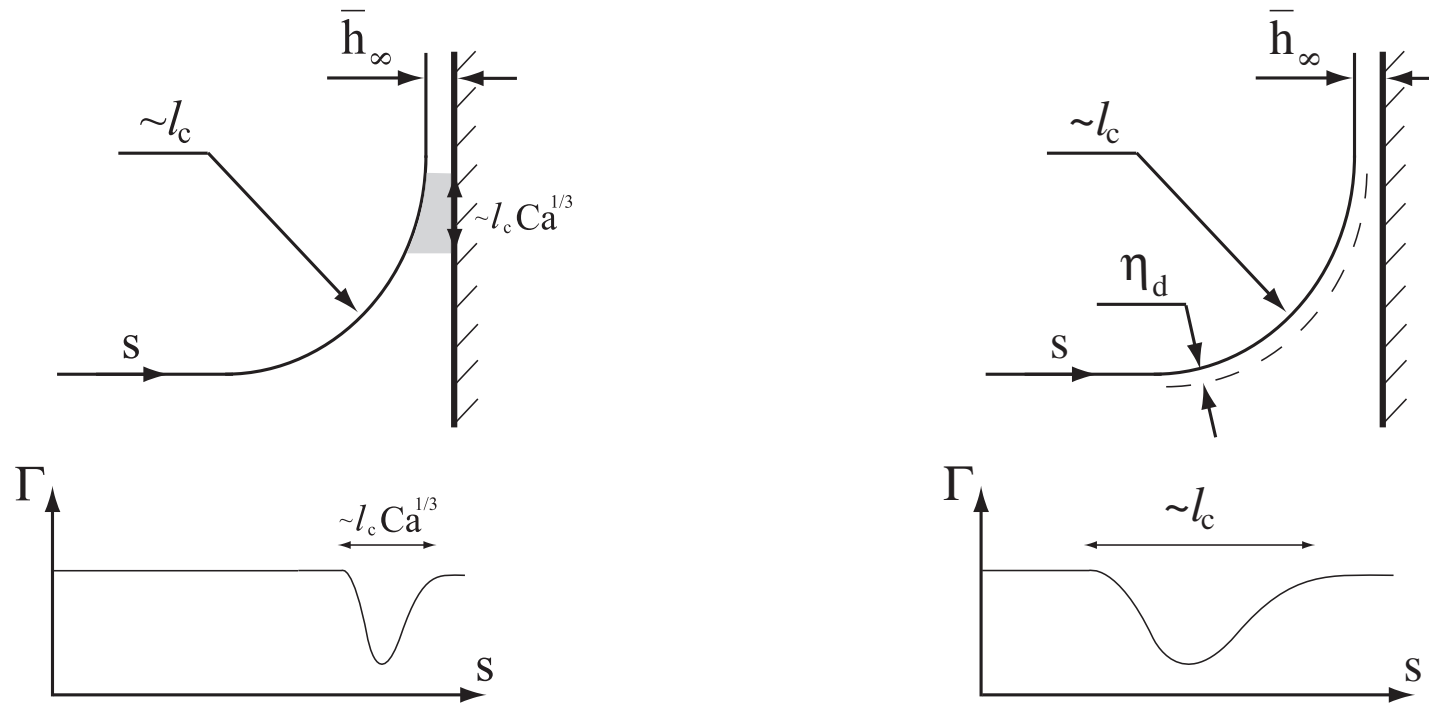
Dependence on Ca for $\Gamma_0 = 0.1$.

Theory: surfactant interface case



Surfactant distribution at the interface for $Ca = 0.1$.

What is wrong with current theories?



Standard asymptotic analysis.

Fully dynamic meniscus.

- Dynamic meniscus: *time of adsorption* $t_a \sim \Gamma_m/k_a C \sim 0.2$ s is of the order of *interface stretching time* $t_v \sim l_c/U \sim 0.2$ s.
- Sorption-limited transport: sublayer is $\eta_d \sim \Gamma/C \sim 1$ μm , thus *diffusion time* $t_{\text{diff}} \sim \eta_d^2/D \sim 10^{-3}$ s is negligible compared to the *adsorption time* $t_a \sim 0.2$ s.

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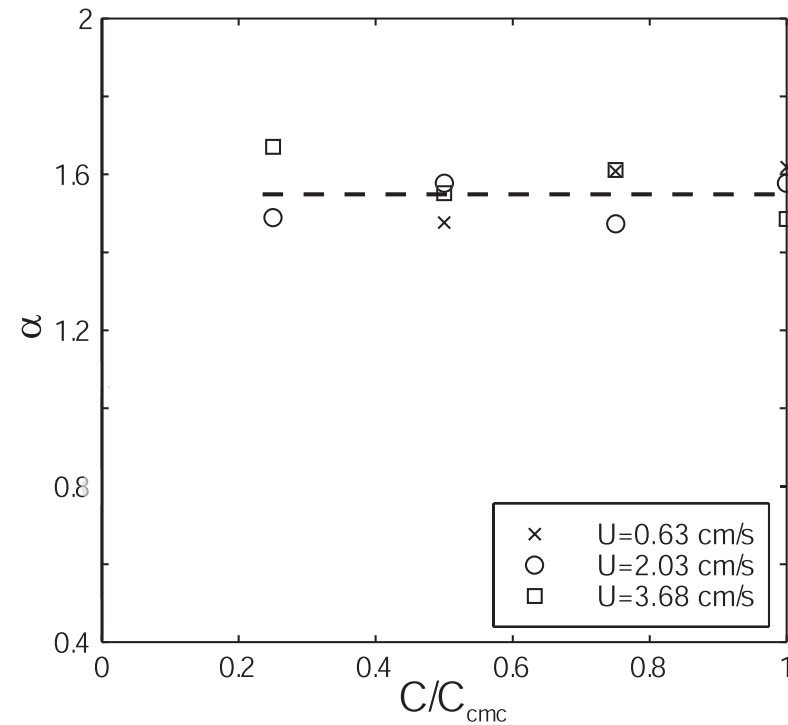
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Conclusions of our theoretical study:

- Pure hydrodynamic modelling of surfactant effect leads to film *thinning*, which contradicts the experimental facts.
- Thus, there are two options:
 - Film thickening **is** due to Marangoni effects, but there is a problem with fundamental equations, or
 - Film thickening **is not** due to Marangoni effects, and the pure hydrodynamic approach based on standard macroscopic equations is not satisfactory to explain the observations.

Experimental study:



Film thickening factor α .

Is the thickening due to Maragoni?

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- As follows from the Langmuir-Hinshelwood kinetics,

$$\frac{d\Gamma}{dt} = k_a C \left(1 - \frac{\Gamma}{\Gamma_m} \right) - k_d \Gamma,$$

with $k_a = 0.64 \cdot 10^{-5} \text{ m s}^{-1}$ and $k_d = 5.87 \text{ s}^{-1}$, Marangoni stresses become negligible if adsorption is faster than the interface stretching, *i.e.* the product $St \kappa > 1$, ($St = k_a/U$, $\kappa = l_c C/\Gamma_m$).

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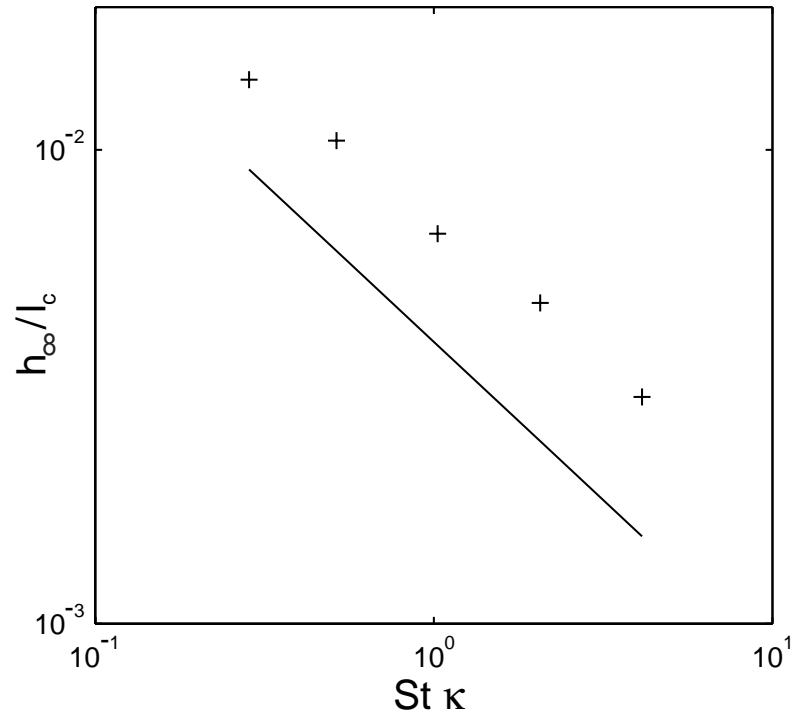
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- As the theory predicts, Marangoni stresses depend on Ca (speed of withdrawal), and thus would distort the 2/3 law.

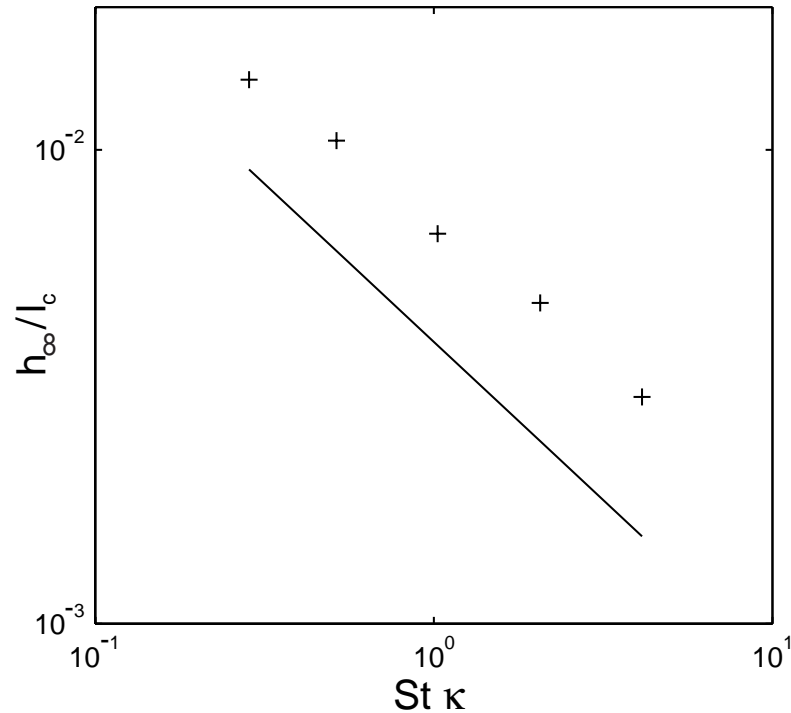
Indication of non-Marangoni origin

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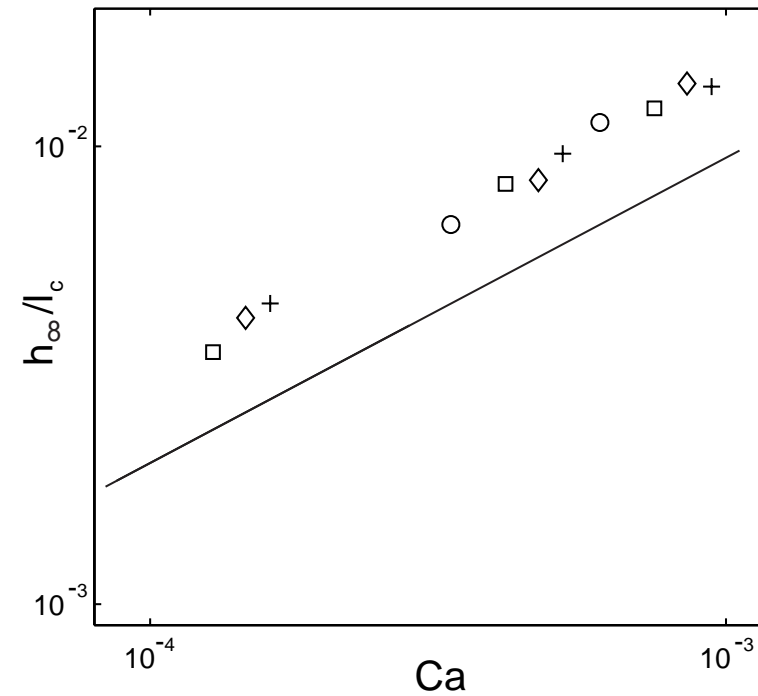


Film thickening in the case of fast adsorption.

Indication of non-Marangoni origin



Film thickening in the case of fast adsorption.



LL law; o, 0.25; square, 0.50; diamond, 0.75; +, 1.00 CMC.

Conclusions on Part III

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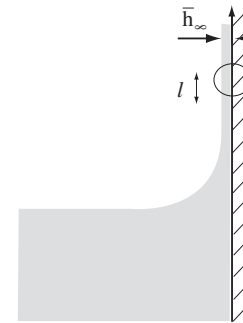
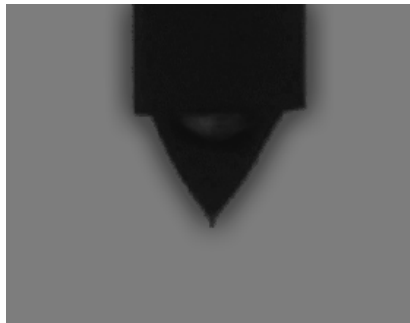
Conclusions on Part III

- Fully nonlinear theory based on a hydrodynamic modeling of surfactant effects yields *film thinning*.
- Experimental study, based on kinetic properties of surfactants, confirmed the non-Marangoni origin of the *film thickening*.
- The above controversy reveals the inconsistency of the existing asymptotic theories, and the lack of an appropriate theoretical explanation.

References

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The end



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